

# Evaporation of Liquid Chlorides in Closed Tanks using the PHOENICS Code

## Presentation of a Rigid Interface Model (RIModel)

Olivier PRAT<sup>1,3</sup> - Jalil OUAZZANI<sup>2</sup> - Olivier BRIOT<sup>3</sup>

<sup>1</sup> QUALIFLOW S.A. – *MONTPELLIER*

<sup>2</sup> ARCOFLUID – *ORLANDO, FL*

<sup>3</sup> GROUPE D'ETUDE DES SEMICONDUCTEURS – *MONTPELLIER UNIVERSITY*

## SUMMARY

- 1 - INTRODUCTION
- 2 - EVAPORATION OF LIQUIDS - *Theoretical Background*
- 3 - RIModel (Rigid Interface Model)
  - *Governing Equations and Characteristics*
  - *Application with the PHOENICS Code*
  - *Boundaries Conditions for Parametric Study*
  - *Simulated Cases*
  - *Exemple of Results*
- 4 - RIModel VALIDITY LIMIT - *Subcooled Pool Boiling Situation*
- 5 - CONCLUSION

## INTRODUCTION

### 1 - Optical Fiber Industry

- Liquid (  $\text{SiCl}_4$ ,  $\text{GeCl}_4$ , ... ) changed into Vapor and Oxydized (  $\text{SiO}_2$ ,  $\text{GeO}_2$ , ... )
- Mainly used Current Technique : Bubbling  $\Rightarrow$  Carrier Gas send into Liquid
- Intended Technique : Direct Liquid Evaporation for Higher Vapor Flow expected

### 2 - Prediction of Evaporation Phenomenon means turn to Numerical Simulation

- Hydrodynamic and Thermal Phenomena Simulation inside Closed Tanks
- Start from Equilibrium Situation and Simulation of Flow Requirements for Optical Fiber Production

## INTRODUCTION

### 3 - Specific Model for prediction of Evaporation Process in closed Tanks

- Multi-Domain Method

  - ⇒ Resolution of each Phase separately

    - ⇒ *Two Phases linked by Boundaries Conditions at the Interface*

- Use CHAM's CFD PHOENICS

  - ⇒ Computation of a Specific Model for Evaporation in Closed Tanks

  - ⇒ Interface taken as a Rigid Plate with a Moving Speed

    - ⇒ *RIModel (acronym of Rigid Interface Model)*

## EVAPORATION OF LIQUIDS - *Theoretical Background*

### 1 - Two kinds of Evaporation Processes for Liquids

- Vapor directly produced at Liquid / Vapor Interface (*Radiative Heating for instance*)
- Vapor produced by Bubbles starting at Immersed Solid Heated Surface (*Pool Boiling*)

### 2 - Pool Boiling $\Rightarrow$ *4 Boiling Mechanisms*

- Subcooled Boiling  $\Rightarrow$  *No bubbles (or Recondense near Heated Surface)*
- Boiling with Net Evaporation  $\Rightarrow$  *Nucleate Boiling Region*  
 $\Rightarrow$  *Partial Film Boiling Region (or Transition)*  
 $\Rightarrow$  *Film Boiling Region*

## EVAPORATION OF LIQUIDS - *Theoretical Background*

### 3 - How to predict Evaporation Phenomenon in Closed Tanks ?

⇒ ASSUMPTION :

*Pool Subcooled Boiling ⇒ Pressure Stability, Avoiding Decay of Liquid Precursors*

⇒ CONSEQUENCE :

*Two Phases Liquid and Vapor strictly separated : Analogy with Melting Process*

⇒ Two Regions with Different Thermodynamic Properties separated by a Moving Interface

⇒ Heat Exchange at the Interface according Heat Conduction with Release (*Solidification or Condensation Process*) or Absorption of Heat (*Melting or Evaporation Process*)

## RIModel - *Governing Equations and Characteristics*

### 4 - Implement Features with PHOENICS $\Rightarrow$ *Rigid Interface Model ( RIModel )*

- *Vapor Quantity Calculation by a Mass Balance and the Perfect Gas Law : **Mvap (t)***

$$M_{\text{vap}}(t) = M_{\text{vap}}(t = 0) - M_{\text{coll}}(t) + M_{\text{int}}(t) \Rightarrow \mathbf{P_{\text{vap}}}$$

- *Liquid Interface Temperature Calculation with Antoine's Equation (  $\text{SiCl}_4$  ) : **Ts***

$$P_{\text{vap}} = 10^{[ 4.09777 - 1200 / ( T_s - 37 ) ]} \Rightarrow \mathbf{T_s}$$

- *Mass Exchange Calculation at the Interface : **qint (t)***

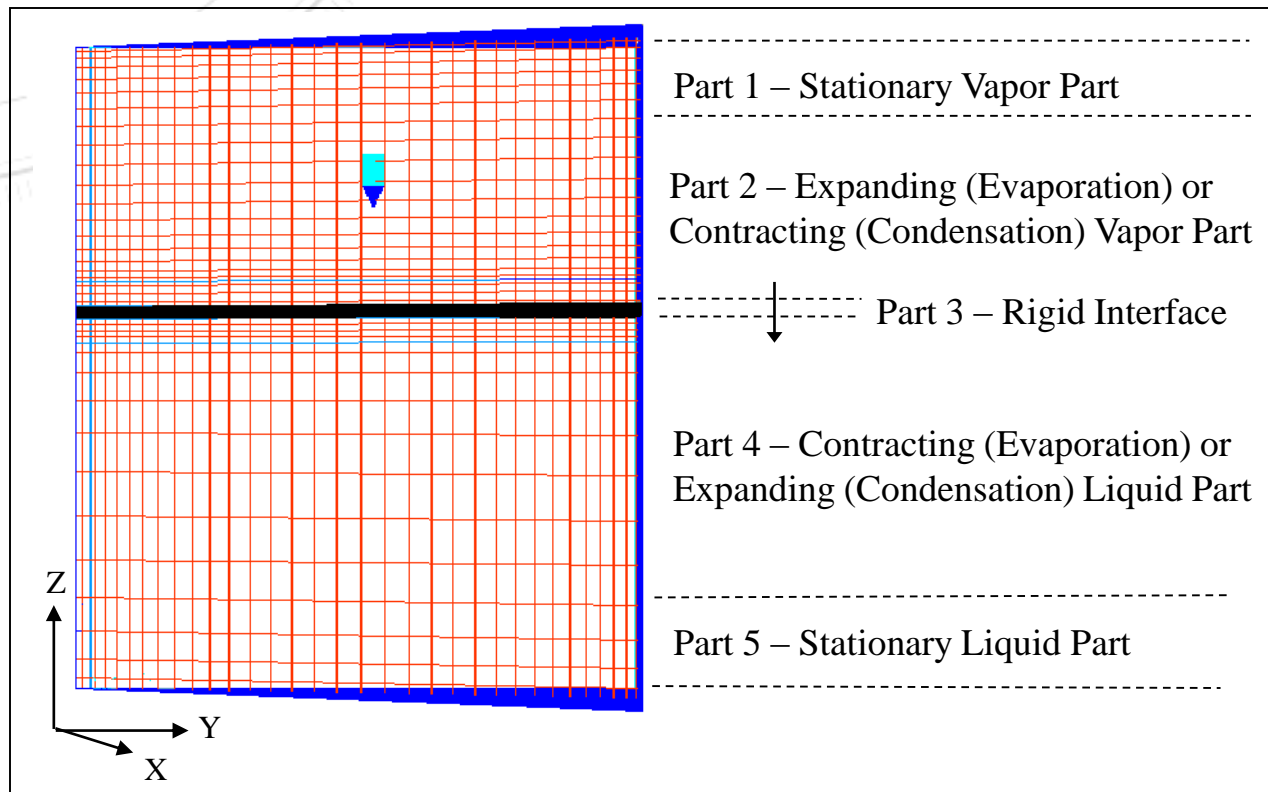
$$q_{\text{int}}(t) \cdot \Delta H_{\text{vap}} = [ \lambda_{\text{vap}} \cdot (\partial T / \partial z) - \lambda_{\text{liq}} \cdot (\partial T / \partial z) ] \Rightarrow \mathbf{q_{\text{int}}(t)}$$

- *Interface taken as Rigid Plate with Moving Speed equal to Evaporation Speed*
- *Friction at the Vapor Side of the Plate and Slip without Friction at the Liquid Side of the Plate*

## RIModel - Application with the PHOENICS Code

1 - Moving Grid Option  $\Rightarrow$  *ZMOVE* function of PHOENICS

2 - Tank Internal Domain splitted in 5 Zones





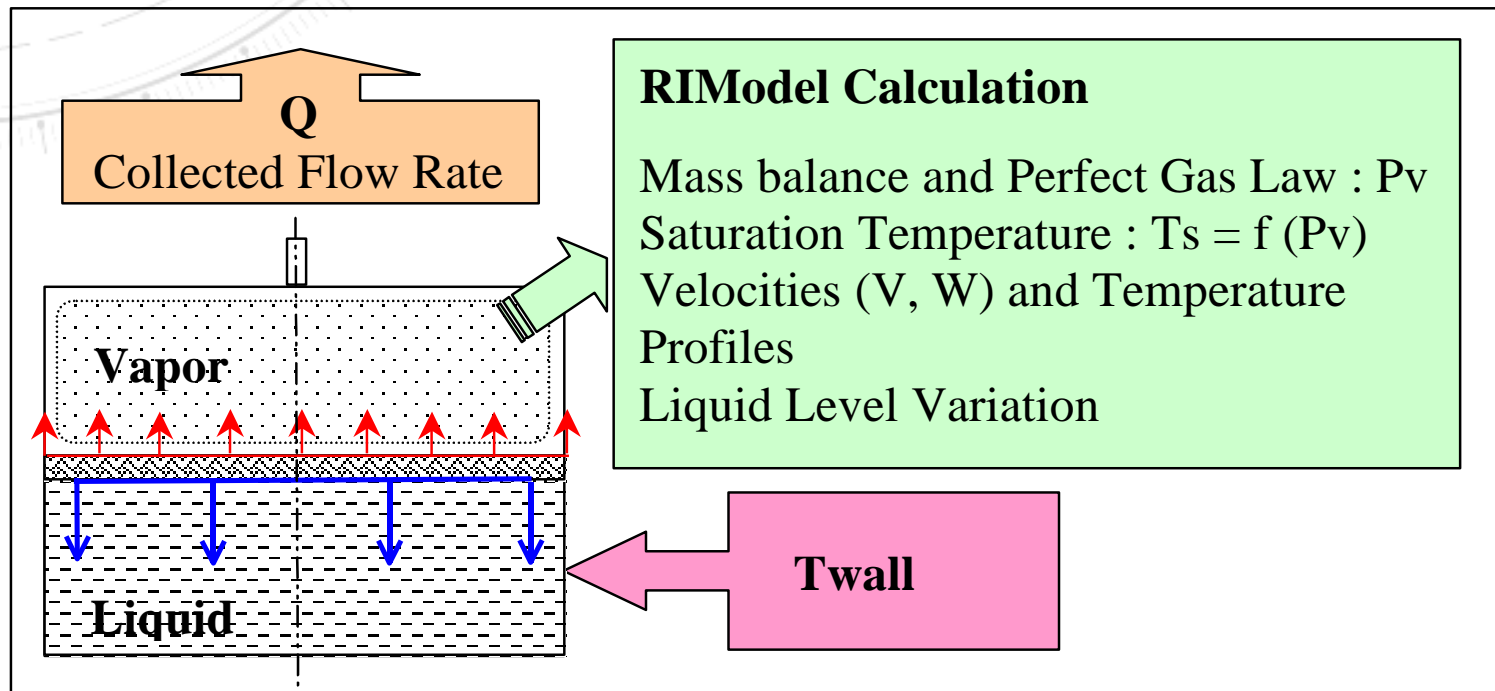
## RIModel - *Boundaries Conditions for Parametric Study*

3 PARAMETERS FOR  
PARAMETRIC STUDY

⇒ **Q** ( *Collected Vapor Flow* )

⇒ **S** ( *Size of Evaporation Surface* )

⇒ **T<sub>wall</sub>** ( *Fixed Wall Temperature* )



**RIModel - *Simulated Cases***

		<b>S1</b>	<b>S2 = 2 x S1</b>	<b>S3 = 5 x S1</b>
		Geometry n°1 ( S1 = 5.6 dm <sup>2</sup> )	Geometry n°2 ( S2 = 11.2 dm <sup>2</sup> )	Geometry n°3 ( S3 = 28 dm <sup>2</sup> )
<b>Q1</b>	Vapour Flow n°1 ( Q1 = 6.5 gr/min )	Case n°1	Case n°4	Case n°7
<b>Q2 = 2 x Q1</b>	Vapour Flow n°2 ( Q2 = 13 gr/min )	Case n°2	Case n°5	Case n°8
<b>Q3 ≈ 5 x Q1</b>	Vapour Flow n°3 ( Q3 = 30 gr/min )	Case n°3	Case n°6	Case n°9

*And for Every Case :*

⇒ Same Tank Internal Volume (29 Liters) and Liquid Quantity (20 Liters)

⇒ Fixed Wall Temperature (T<sub>wall</sub>) fixed by “Empiric” Determination

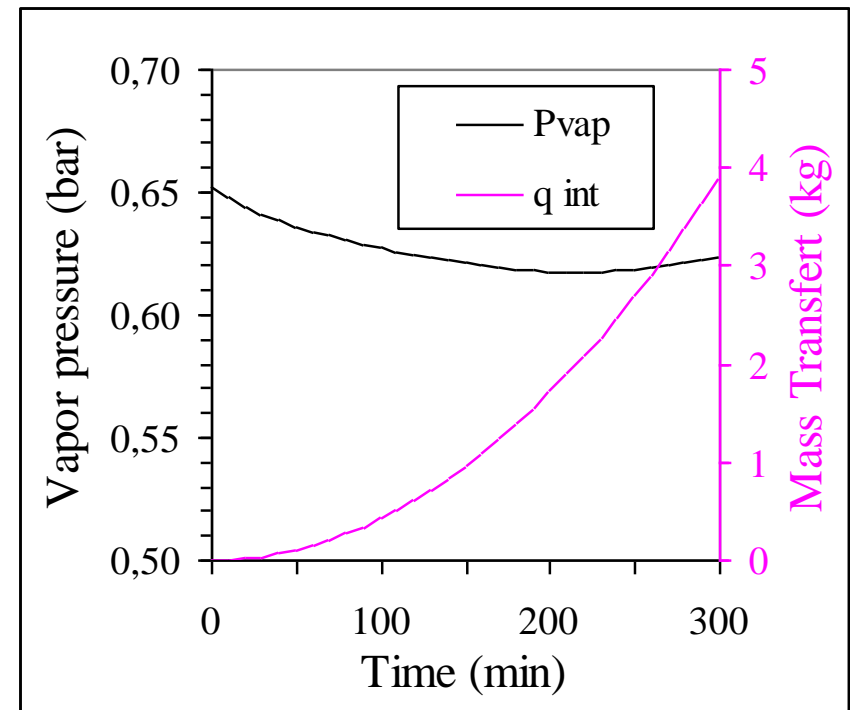
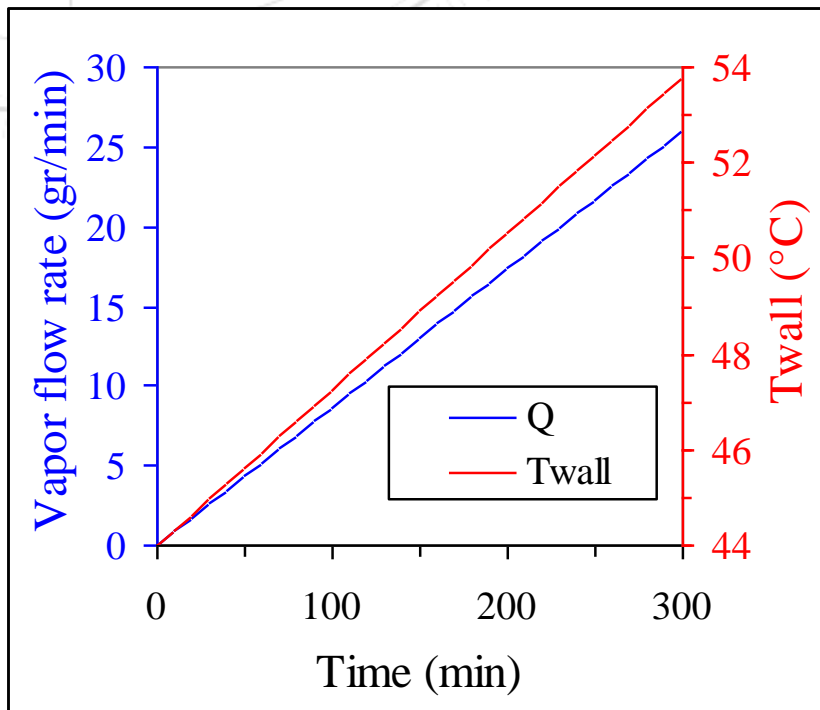
## RIModel - *Exemple of Results for Case n°5*

### 1 - Boundary Conditions

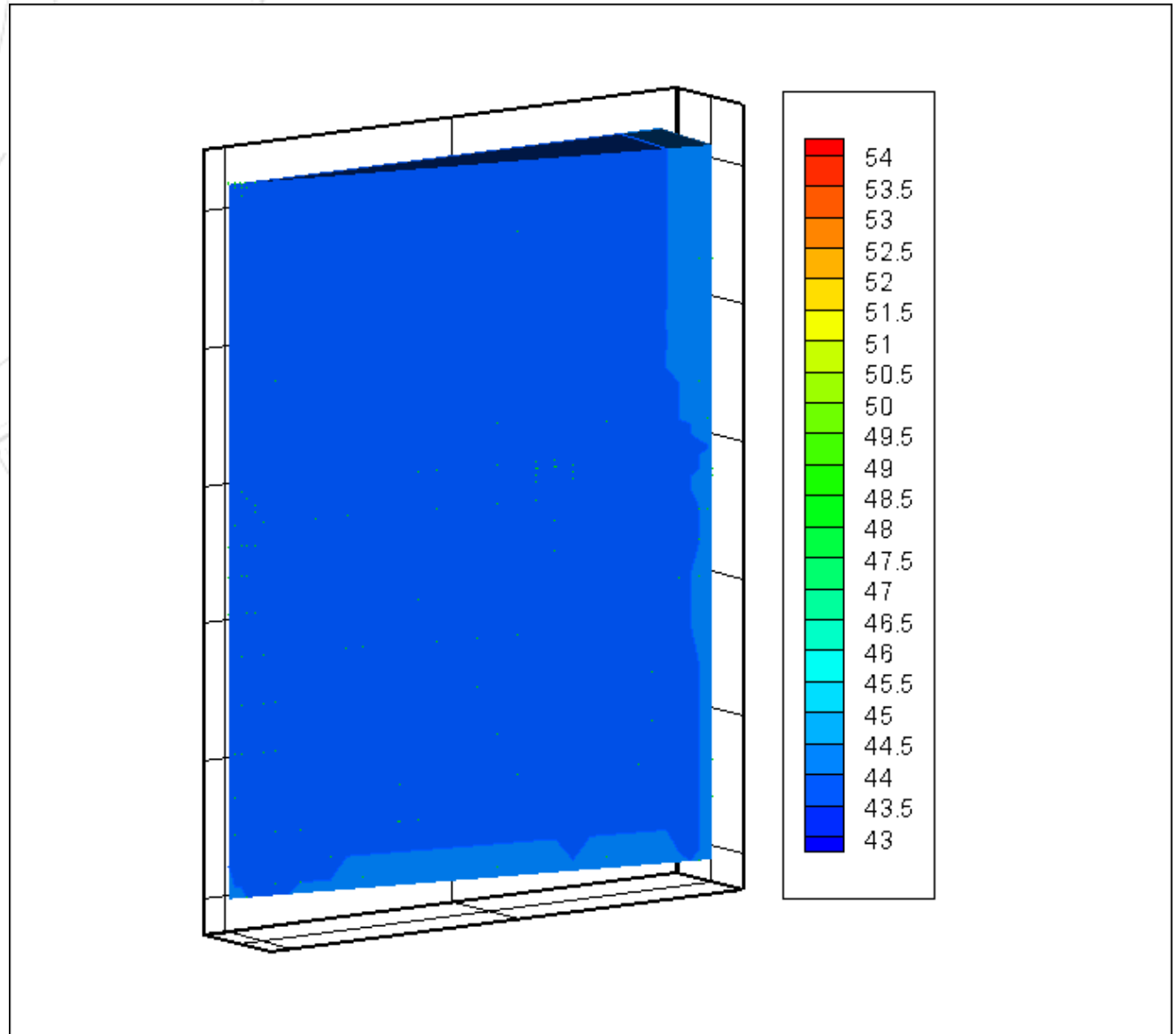
- ⇒ *Collected Vapor Flow :  $Q_2$*
- ⇒ *Evaporation Surface :  $S_2 = 11.2 \text{ dm}^2$*
- ⇒ *Fixed Wall Temperature :  $T_{wall}$*

### 2 - Simulation Results ( start from $44^\circ\text{C}$ )

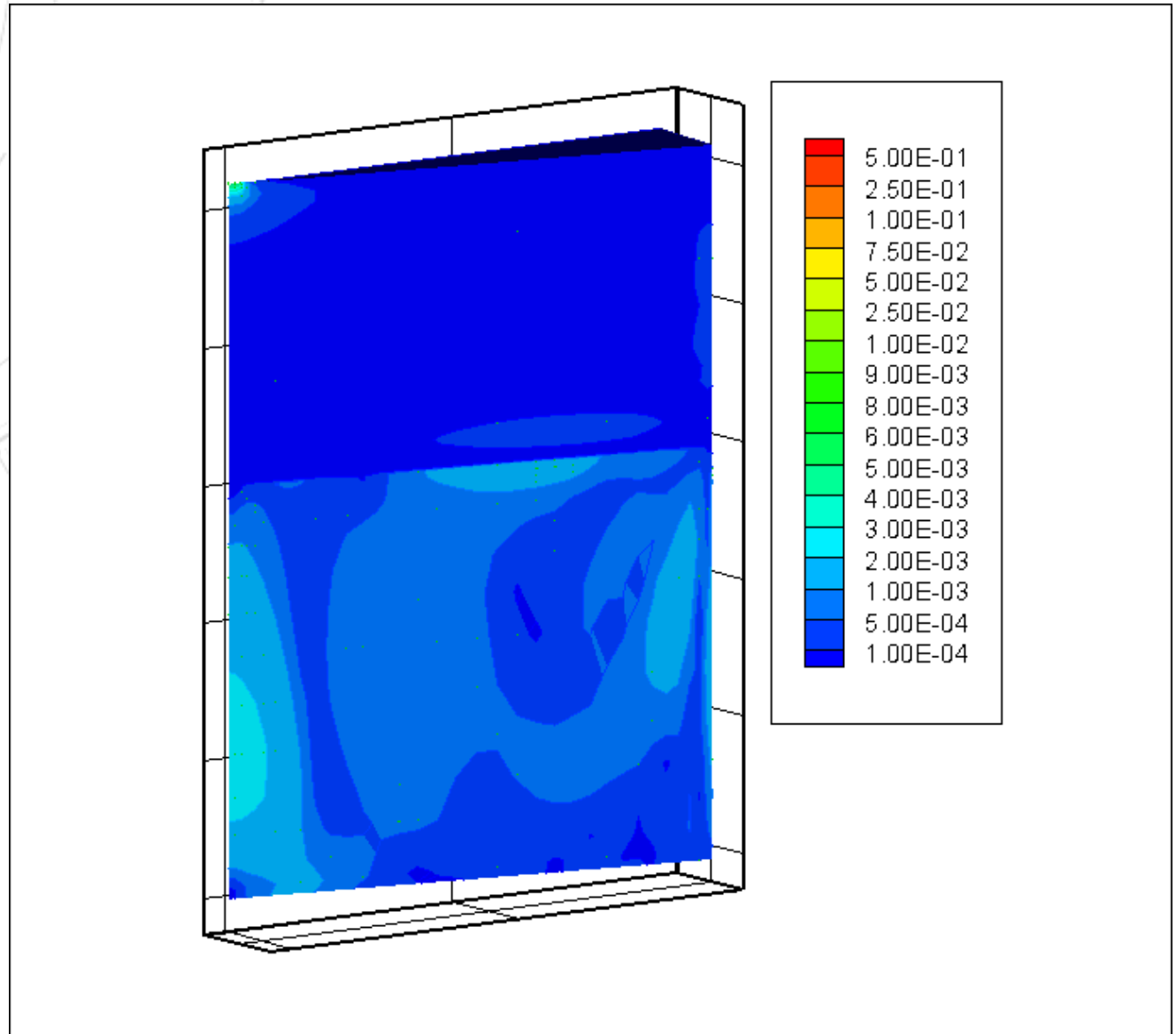
- ⇒ *Vapor Pressure :  $P_{vap}$*
- ⇒ *Interfacial Mass Transfert :  $q_{int}$*



Temperature



Velocity



## RIModel VALIDITY LIMIT - *Subcooled Pool Boiling*

1 - The RIModel  $\Rightarrow$  *Assumes Pool Subcooled Boiling Situation*

2 - The Transition Pool Subcooled Boiling to Nucleate Boiling

$\Rightarrow$  *Depend on Gap between Wall and Saturation Temperatures*

$$\Delta T = T_{\text{wall}} - T_{\text{sat}} = [ 2 \cdot \sigma \cdot T_{\text{sat}} ] / [ \rho_{\text{vap}} \cdot \Delta H_{\text{vap}} \cdot R ]$$

$\Rightarrow$  *Depend on Nucleation Cavity Radius*

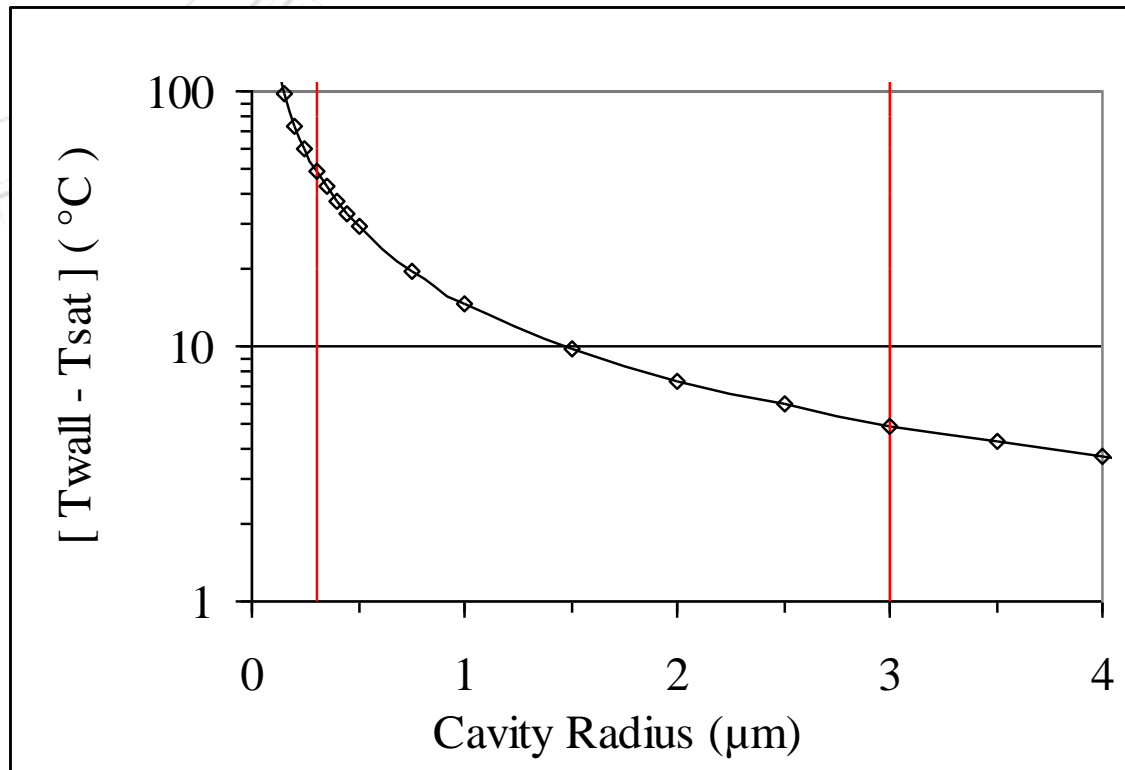
3 - Typical Cavity Radius in the  $\mu\text{m}$  Range

$\Rightarrow$  *0.3  $\mu\text{m}$  < Cavity Radius : R < 3  $\mu\text{m}$   $\Rightarrow$  50  $^{\circ}\text{C}$  >  $\Delta T$  > 5  $^{\circ}\text{C}$*

$\Rightarrow$  *CONSEQUENCE : RIModel valid for Temperature Gap of about 20 $^{\circ}\text{C}$  (and even more : no major disturbance induced by Beginning of Nucleate Boiling)*

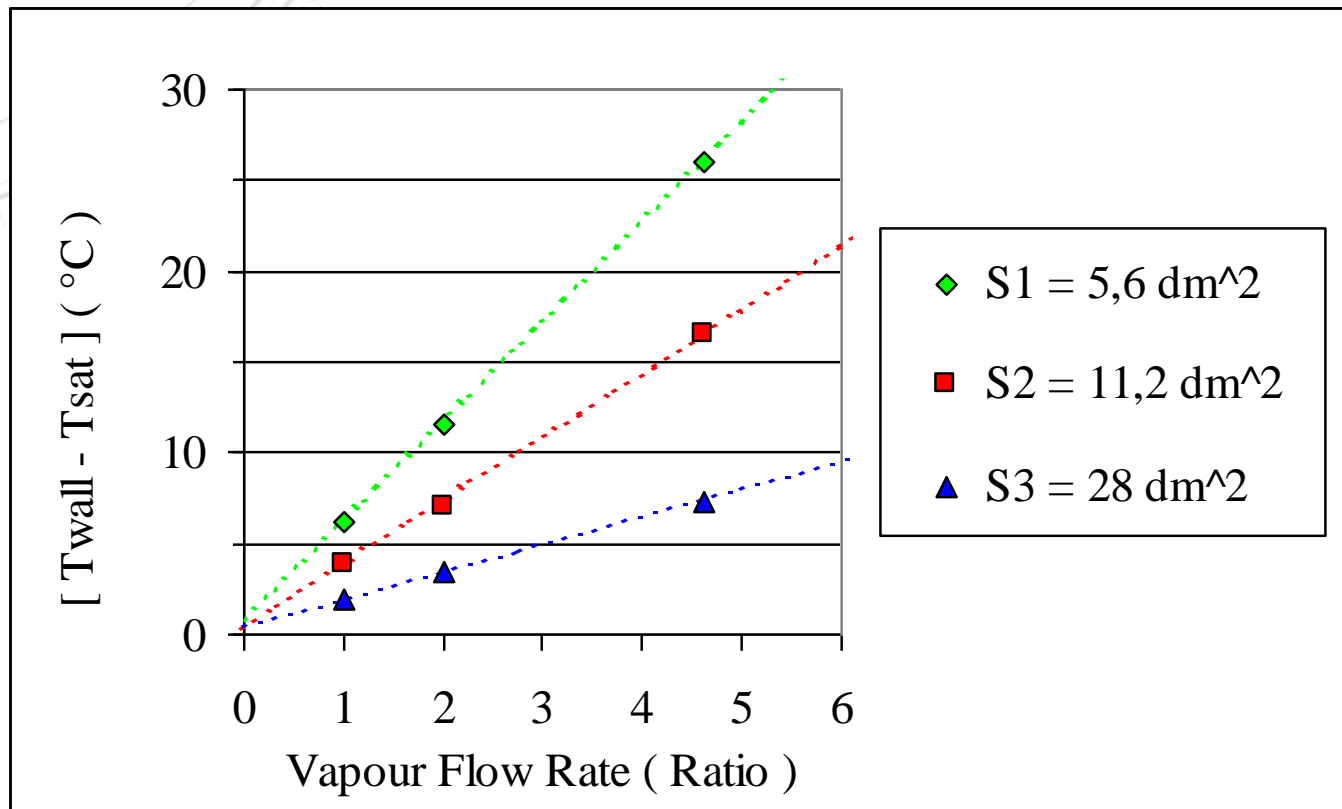
## RIModel VALIDITY LIMIT - *Subcooled Pool Boiling*

⇒ Onset of Heterogeneous Nucleation ⇒  $\Delta T = f(\text{Cavity Radius})$



## RIModel - Parametric Study Results - Temperature Gap

⇒ Temperature Gap Dependence with Vapor Flow Rate (  $Q$  )  
and Evaporation Surface Size (  $S$  )





## CONCLUSION

### 1 - The RIModel for Evaporation of Liquids in Closed Tanks is :

- ⇒ Based upon Heat Conductivity at Liquid / Vapor Interface by analogy with Melting or Solidification Process
- ⇒ Assuming Pool Subcooled Boiling Situation
- ⇒ Assuming to preserve Plane Interface during Evaporation

### 2 - The Parametric Study ⇒ *Quantify influence of Boundary conditions ( $Q$ , $S$ , $T_{wall}$ )*

- ⇒ For same couple (  $Q$ ,  $T_{wall}$  ) ⇒ The larger (  $S$  ) ⇒ The bigger (  $P_{vap}$  )
- ⇒ For same couple (  $Q$ ,  $P_{vap}$  ) ⇒ The larger (  $S$  ) ⇒ The smaller (  $T_{wall}$  )

### 3 - Critical discussion of Numerical Results

- ⇒ With features of Boiling Process and Mechanism of Bubbles Generation
  - ⇒ *RIModel Limit of Validity*